

# INVESTIGATION AND REPORT

ON THE

# MANUFACTURE OF DESSICATED MILK

BY THE

# ANDREWS PATENT PROCESS

AS COVERED BY

UNITED STATES PATENT NUMBER 1,012,578

AND BY MANY FOREIGN PATENTS

FREDERIC BUCH

ENGINEER

43 EXCHANGE PLACE, NEW YORK CITY

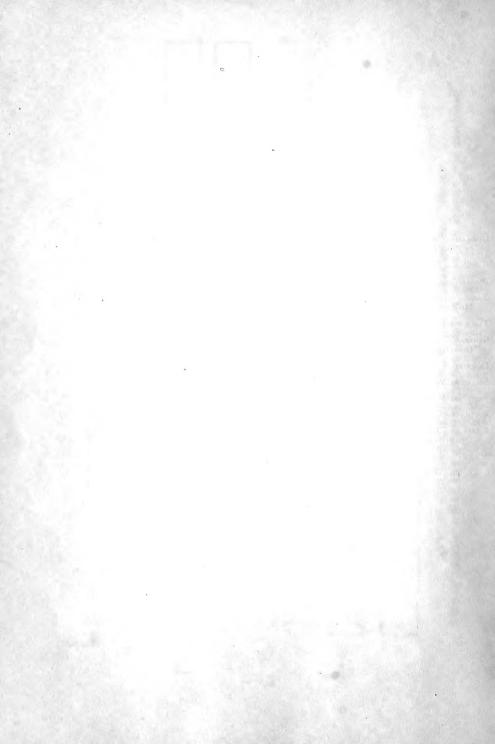
NOVEMBER 1, 1913

COPYRIGHTED, 1913, BY HARRY IRVING ANDREWS.

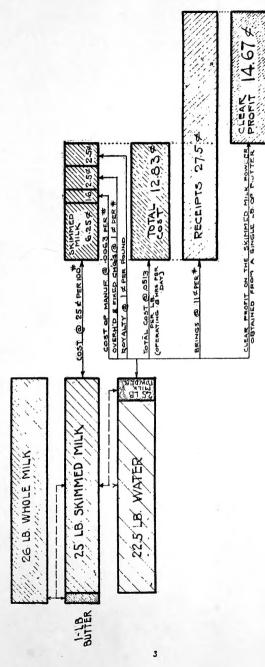


# INDEX

DIAGRAM—WHOLE MILK REQUIRED TO PRODUCE ONE POUND OF BUTTER—SKIMMED MILK REMAINING—COST OF REDUCING SAME TO MILK POWDER—CLEAR PROFIT	3
How Milk Powder is Made	4
DIAGRAMATIC LAYOUT OF A TYPICAL MILK POWDER PLANT AND TABLE SHOWING ROUTING OF MILK	5
Table of Operating Costs and Clear Profits Per Day for Reducing any Quantity of Skimmed Milk up to 60,000 Pounds Per Day	6
Table for Estimating Clear Profit on One Plant P.	7
General Expenses: Estimated Overhead and Fixed Charges Per Plant, Per Day—Other Estimated Operating Costs Per Day	8
Description of Evaporator.	9
SECTIONAL VIEWS OF EVAPORATOR.	10
Sectional Views and Description of Drum	11
Estimated Cost of One Plant.	11
Chart for Determining Amount of Horse Power Required and Running Hours of Plant for any Quantity of Milk up to 60,000 Pounds Per Day	12
MILK POWDER PLANT—PLAN AND ELEVATION.	13
Some Milk Powder Products	14



# DIAGRAM SHOWING WHOLE MILK REQUIRED FOR ONE POUND OF BUTTER AND SKIMMED MILK REMAINING, TOGETHER WITH VARIOUS COSTS, AND THE PROFITS FROM THE MILK POWDER.



The figures in this diagram are based on an 8-hour day of operation. It will be seen that with

Skimmed milk at 2.5 c per 10 ths. (=1 th. powder.) Cost of man'f're .63c per th. of powder. Overhead and fixed charges. 1.00c per th. of powder. And royalty.... 1.00c per th. of powder.

For 2.5 fbs. we have  $5.13\times2.5=12.83c$  total cost. Selling the powder at 11c per 15,-2.5.41=27.5c. Profit on 2.5 fbs. of milk powder made from 25 fbs. of skimmed milk is 27.5-12.83=1467c.

5.13c cost per tb. of powder.

0

# HOW MILK POWDER IS MADE

# TYPICAL MILK POWDER PLANT

By referring to the accompanying diagram a comprehensive working knowledge of a milk drying plant will be had, the diagram showing a layout of the machinery, apparatus, vats, tanks, etc., through which the milk must pass from the time it first enters the plant until it is packed in barrels, boxes, or cartons; the finished product, ready for shipment.

# PROCESS OF MANUFACTURE

Milk enters the plant immediately after being weighed on the wagon scales and is dumped from the milk wagons so that it will flow by gravity into cold storage vats, where it is accumulated until the quantity becomes sufficient to start the plant. The milk is then caused to flow into a regulating tank, located just above the cream separators, as shown. By means of this tank the flow of the milk into the separators is adjusted and controlled as desired.

Milk and cream are now separated, and, if butter is to be made, the cream led to a cream storage tank and thence to the butter-making machinery, while the skimmed milk passes through a degermer where bacteria is destroyed and the milk purified by a patent process.

The skimmed milk now passes into the main evaporator, where evaporation is affected until it becomes about the same consistency as the pure cream in the cream tank, or ordinary condensed milk.

This condensed milk now flows into the mixing or revitalizing tank, where it is revitalized by the introduction of pure filtered air, and, if no butter is to be made, the cream and condensed milk are here united.

The two, now being of the same consistency, may be forced together into the secondary evaporator or drum, where the remaining moisture is quickly evaporated and carried off, the milk and cream, or milk only, now forming chips or strips of a yellowish appearance.

These milk strips and chips, being very damp, are next passed into a tumbler directly under the drum, where they are broken into particles and brought into contact with hot dry air, to be dried out as completely as possible before being allowed to enter the pulverizer or grinder, for the final grinding into milk flour or powder of a suitable fineness desired by the trade.

That nothing may be lost or wasted, the grinder is enclosed in an air-tight casing and connected by a powerful suction fan to a dust collector, where every particle of the powdered milk is collected and then allowed to flow into barrels or boxes to be removed to the store room or shipping platform.

For this purpose a mechanical conveyor may be brought into use if desired, as indicated in the diagram, but as the average grinder or pulverizer now on the market could hardly produce more than one barrel (360 pounds) of powder per hour under the most favorable conditions, it will be seen that a conveyor is hardly a necessity.

From the foregoing it will be seen that, if based on the right principles, the process is simple indeed, and that if the machinery is properly designed and proportioned no skilled labor will be required, as everything is arranged to work automatically and with a mechanical precision that smirks of the best efforts of the trained or skilled hand.

# THE ACCOMPANYING TABLE

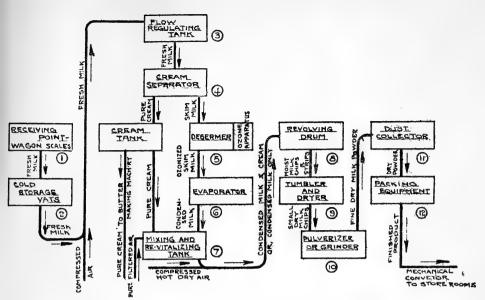
To give a still clearer outline and better understanding of the process just described, the table under the diagram has been added. The consecutive numbers in the first column give exactly, in running order, the routing of the milk through the plant, while the second and third columns give the names of the various apparatus or parts, and their respective functions.

# OTHER MECHANICAL EQUIPMENT

Engine and boiler, air heater and dryer, air compressor, the various piping systems and other minutae have been purposely omitted from the diagram as the interest here is centered on the process of manufacture rather than on mechanical details, which in some instances need but slight consideration, as they already form part of a plant to which the milk powder machinery may be added.

Note.—If this process was not based on the right principles, the German patent would not have been allowed —and the German Government protects its basic patent grants.—Inventor.





# DIAGRAMATIC LAYOUT OF APPARATUS AND PIPING FOR COMPLETE MILK POWDER PLANT

SHOWING EXACT TRAVEL OF MILK IN BEING TREATED HOTE - ARROWS INDICATE DIRECTION OF FLOW.

	Table 1.—Routing of Milk					
NUMBER	MACHINERY OR APPARATUS	FUNCTION				
1	Wagon Scales.	Weigh milk as received.				
2	Cold Storage Vats.	Store and preserve milk until needed, or until quantity becomes sufficient to start plant.				
3	Flow Regulating Tank.	Regulate and adjust flow of milk into the cream separators so the latter cannot choke or become overloaded.				
4	Milk and Cream Separators.	Separate cream from milk so that the former may be used for butter and the latter for milk powder products, or the two brought to the same consistency to be reduced to powder together.				
5	Degermer.	Purify milk and kill bacteria without causing coagulation or destroying life and protein as is the case with pasteurizing.				
6	Evaporator.	Evaporate principal moisture from the skim milk and reduce it to the same consistency as pure cream without causing boiling or burning of the milk.				
7	Mixing and Re-vital- izing Tank.	Re-unite and re-vitalize cream from separators and condensed milk from evaporators by the introduction of pure filtered air.				
8	Revolving Drum or Secondary Evaporator.	Complete evaporation of moisture from re-vitalized condensed milk, or from combined milk and pure cream.				
9	Tumbler and Dryer.	Break up into small particles, and dry out evaporated product, and prepare same for pulverizer or grinder.				
10	Putverizer or Grinder.	Grind dried product to desired fineness.				
11	Dust Collector.	Forcibly collect from pulverizer, by powerful air suction, every particle of milk powder or flour and chute it into barrels, boxes, cartons, etc.				
12	Packing Equipment.	Suitable arrangement for sealing barrels or boxes and transferring them to store-rooms or shipping platform by means of mechanical conveyors.				



# Table of Operating Costs and Clear Profits Per Day

	18	10.00-00-0	- Notic 10 h	σ. Φ. Φ. Ο	- N m 4-10	U 1-00 00
MILK.	CLCAR PROFIT PER DAY OVER ALL EXPENSES	20.05 34.36 48.67 77.21		206.08 220.39 235.50		320.2c 334.27 348.28 362.29
10	GROSS RECEIPTS PER DAY @ 11 & GER LB.	110.00 (32.00 154.00 176.00 198.00	242.00 264.00 286.00 308.00 338.00 335.00	396.00 418.00 440.00	462.00 484.00 506.00 528.00 550.00	572.00 594.00 616.00 638.00
MTITIE	TOTAL COST PER LB.	0899 1800 1700 1700 1700	.062 .0 59 .0 57 .0 57 .0 57 .0 55	.053 .052 .051	120. 050. 040. 049.	840. 840. 840.
WITH VARIOUS QUANTITIES	TOTAL COST PER DAY	83.95 97.64 105.33 113.02 120.71	136.09 143.78 151.47 159.16 166.85 174.54	189.92	212.39 220.68 228.37 236.06 243.75	251.74 259.73 267.72 275.71
JARIO	ROYALTY	0 447000 0	22.00 24. 26. 30.00 34.	% <b>₽</b>	42.00. 44. 46. 48. 50.	52.08 54. 56.
TH	OVERNÍP Z FIXED CHÍSÍS	40.00	40.00		1.50 40.00	11.80 40.00 12.10 ". 12.40 ". 13.00 ".
		5 = = = +	8 = 4			2.34 11.80 2.43 12.10 2.52 12.40 2.61 12.70 2.70 13.00
PLANT	COST COST OF OF S	. 545 . 53 . 53 . 63	.98 1.08 1.26 1.35 1.44 1.53	1.62	1.89 1.98 2.07 2.16 2.25	2.34 2.52 2.52 2.61
ONE	COST OF SKIM. MILK	25.00 35. 45.	-, 0 9 1 . 1	8 % 5	105.00 110. 115. 125.	5.60  3900  6.20  35.  6.80  40.  7.40  45.
FOR O	(05T	6, 64.4.7.9 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	64.7.86 6.4.86 6.4.86 6.20 6.20 6.20 6.20 6.20 6.20 6.20 6.2	10.80 11.40 12.00	13.20 105.0 13.20 110. 13.80 115. 14.40 120. 15.00 125.	
	TOTAL ACTUAL H.P. COMSUMED	150 180 240 270 300	3360 3360 3360 4720 4720 4730 4730 514	540 570 600	630 630 630 720 750	780 810 840 870
PROFIT	7	9 14 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	220 240 260 280 300 320 340	0 8 8 0 0 0 0	440 440 460 500	520 540 560 560
CLEAR	HORSE POWCA CONSLIMED PLANT PULVE- EKCEPT RIZER	80 80 90 90 90		8 8 8 8 8	210 220 230 240 250	272 200 290 390
1 1	ME RS PULVE- RIZER	8.0 8.0 12.0 13.0 13.0	14.6 16.0 17.3 18.6 20.0 21.3 22.5	25.30		34.6 36.0 37.3 36.6
SES or	MACHINE HOURS PLANT- PULVE EXCEPT RIZER	ए जुना क्षा क्ष् ठ देवा जा के	44000 00 40000 40	7.2 8.6 8.0	4.00 00 0 4.00 0 0 6.00 0 6.00 0 6.00 0 6.00 0 6.00 0 6.00 0 6.00 0 6.00 0 6.00 0 7.00	0 0 : : : : : : : : : : : : : : : : : :
EXPENSES and	FINISHED POWDER IN POUNDS	1200   1200   1400   1600   1800   2000		3600 4000 9000	4200 4400 4600 5000	5200 5400 5640 5640 5640
1 1	JPPLY GUARTS	5 50 0 6 60 0 7 60 0 8 60 0 9 60 0		18 000 13 000 20 000	21 000 22 000 23 000 24 000 25 000	26 000 27 000 28 000 25 000
OPERATING	MILK SI	10 000 12 000 14 000 16 000 20 000	22 000 24 000 26 000 28 000 30 000 34 000	36 000 40 000	42 000 44 000 46 000 50 000	52 000 54 000 56 000 58 000
	HUMBER OF 4 HA SMUA	-		Ø		m

Nore.—To find number of cows required to produce a given quantity of milk powder, divide quarts in quart column by 12. Example: 5,000 divided by 12 (the average per day, per cow) and we find 417 cows will produce 1,000 lbs of powder; 30,000 divided by 12, or 2,500 cows, making 6,000 lbs.



# Table for Estimating Clear Earnings for One Plant Per Year

TILK	RUMMING					201	II	S					
SUPPLIED NO.		-	2	2	4	5	บ	7	ထ	8	ō	-	12
0 7 4 3 8 6	0 4 8 0 0 0	6/5. /030. /462. /889. 23/6.	00000000000000000000000000000000000000	745 3030 4336 5667 8447	2474 2478 2024 2024 2024 2024 2024 2024 2024 202	3075 57.50 73.10 9445 17.580	36.90 6/80 877.8 83.34 686.6 98.6 98.6	7270 7270 7270 72234 76273	4920 9240 11696 15112 18528	5535 9270 13158 17001 20844	6150 10308 14628 18894 23163	6768 11330 16082 20799 25476	7380 17544 22668 26732
22 000 24 26 28 28	44000	3/77. 3606. 4033.	6354 7272 8070 8930 9788	953/ 08/8 72/05 73335 73335	1 , 1 / /	15385 18030 20175 22325 24470	1 / Maine	1 '''		28593 32454 46185 40185	37773 36066 40359 44652 48652	34947 39666 44385 49175 53834	38 124 43272 48 420 53 580 58 728
34 34 34 34 34 34 34 34 34	30,77.8 40000	5323. 5750. 6/82. 6611.	10646 11500 1354 13364 14737	15969 17250 18546 19833 21,195	27 292 23 800 24 728 26 778 26 778	26615 30900 33955 33955 35355	3/938 34500 37092 42390	37261 40250 43274	42584				
42 000 44 46 46 50 000	ရာရာပု.ပုဒ် နေ ဆာလျက် 0	7470. 7899. 8328. 8758. 9787.	14940 15798 16656 17516	72410 23697 24984 26274	29.880 31.596 33.372 35.032	37350 39495							
52 000 54 56 58 60 000	ō ō = = -i, 4 ∞ α α ο ο	9607 10028 10048 12868 12868	792/ 2005/ 2005/ 2005/ 2730 300 300 300 300 300 300 300 300 300										

If the milk supply is 40,000 fbs, for 3 months, 38,000 fbs, for 2 months, 36,000 fbs, for 1 month, 30,000 fbs, for 1 month, 20,000 fbs, for 3 months, with the plant lying idle the other 2 months, what should be the clear profits for the year?

# ANSWER-

	\$21,195	13,222	6,182	4,894	8,244
	we find	"	"	,,	ä
	months	,,,	"	3	3
	3	2	ш	_	3
	. under 3	,,	,,	,,	33
	fbs. 1				
	40,000	38,000	36,000	30,000	20,000
1	Opposite	"	33	23	u

	2		
•			
•			
•			
,			
			-

# GENERAL EXPENSES

# Overhead and Fixed Charges

Salary of principal	\$6.00
Traveling expenses of principal	4.00
Advertising	
Gifts to customers	.50
Interest on capital (5% on \$7,000)	1.00
Interest on borrowed money	
Rent (assumed at 8% on value of	
property)	2.63
Stationery, postage, telephone, tele-	
graph	.50
Insurance:	
Fire—\$30 per 1,000 on \$12,000	
property	1.98
Credit	2.00
Partnership	
Casualty	
Bonds	
Liability	
Depreciation of plant	1.00
Repairs	1.00
Unjust claims of customers (1% on	
\$100,000)	2.73
Damage, loss, freight and express	
charges on returned goods	
Collections	2.73
Bad debts	2.73
Factory supplies and equipment	2.00
Office supplies and equipment	.50
Lighting	.50
Taxes (assumed at \$18 per M)	.35
Legal expenses	.50
Maintaining three horses	1.50
Refrigeration	5.00
Charity	.50
Miscellaneous expenses	.35
_	<del>-</del>

Total \$40.00 per day.

Note.—The above is a fair estimate for average conditions. Close inspection may show, however, that not all the items taxed above will enter in every condition, and the overhead and fixed charges may therefore be even less than the quoted \$40.00 per day.

# **Various Operating Charges**

L	LABOR		
	Machinist in charge \$4.00 salary	<i>7</i> .	
	Night watchman		
	Fireman 2.50 per da	ay.	
	Driver		
	Men at grinders—2		
	at \$2.50 5.00 per 10	O-hour day or less.	

# Total \$11.50

ESTIMATED HORSEPOWER— Evaporator	1 10 10	.p
Pulverizer or grinder		"
Total, with 1 grinder		

# COST OF FUEL-

Coal assumed at \$5.00 per ton of 2,000 lbs. Eight (8) lbs. of coal per h. p. per hour. This gives cost of coal at 2 cents per h. p. per hour.

# MILK SUPPLY-

Price of skimmed milk assumed at 25 cents per 100 lbs.

# BARRELS FOR PACKING FINISHED POWDER—

Barrels assumed at 15 cents each when bought in lots.

360 tbs. of powder per barrel, 2.77 barrels per 1,000 tbs.

This gives 411/2 cents, say 45 cents, per 1,000 fbs.

# ROYALTY-

In order to obtain the exact clear profit, over and above all ordinary possible expenses, the royalty is here included with the operating expenses.

The royalty amounts to one (1) cent per pound of milk powder.

-		
•		

# **EVAPORATOR**

The evaporator shown in the accompanying illustration serves to reduce skimmed milk to the consistency of condensed milk, by evaporating about 75% of the moisture. This should be accomplished without the milk reaching 156 degrees F, as at that temperature the albumen is coagulated and a cooked taste acquired.

In the Andrews System this difficulty is overcome by rapid alternating heating and chilling of the milk, instead of a heating process alone (as is the case in all other methods, none of which are a complete success), the slight chilling always occurring just as the milk reaches the maximum allowable temperature before boiling or burning, thus automatically preventing overheating of the same.

The illustration shows the evaporator in section, both from the front and side. It consists mainly of a sheet metal casing carried by an angle iron frame made up practically air-tight, with inlet pipes at the top for the skimmed milk to be treated, and outlets at the bottom through which the condensed milk passes to the re-vitalizing tank. There are also large inlet and outlet connections for the hot dry air used to absorb and carry off the moisture evaporated from the milk.

Access doors are provided on three sides for cleaning and inspection purposes. These are closed airtight when the evaporator is in operation.

The perforated spread pipes at the top serve to evenly distribute the incoming milk. The slightly inclined corrugated plates directly under the spread pipes are of wired glass for sanitary reasons. Their purpose is to heat the milk to a certain desired temperature so that evaporation may immediately commence when the liquid strikes the upper hot rollers. The plates are heated from the iron pipe coils shown directly underneath.

The rollers, over which the milk must pass, are also of wired glass, or, they may be made of cast iron with a heavily nickeled surface to resist the corrosive action of the heated milk. They are hollow so that steam or electric heat and ammonia gases may be passed through alternate rollers, thus causing a perfect hot and cold process for treating the milk.

The inlet pipes to these rollers are fitted with thermometers, pressure gauges, and instantly adjustable pressure regulating valves, thus allowing the minutest adjustment of temperatures. The rollers rotate with the inlet and outlet pipes acting as the shafts—they are driven by a sprocket chain on the outside of the casing.

Each roller is fitted on the under side with an automatic scraper, held tight against the same by adjustable springs. These springs prevent the milk from clinging to the surface of a roller beyond the specified time.

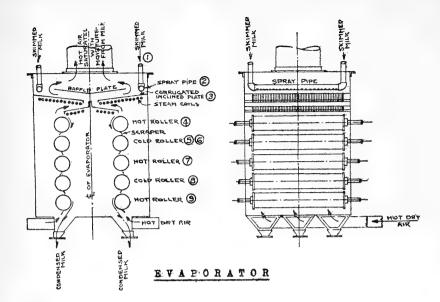
The machine is so proportioned that the layer of milk on the surface of the upper rollers will be approximately 1/32" in thickness, while on the successive rollers it will necessarily be proportionately less. The temperatures and speed are carefully adjusted at the first operation and are thereafter constant, making the entire process of evaporation a mechanical one with no need for skilled or specially trained help.

The rotating pipe ends of the rollers are connected to the inlet and outlet pipes with special stuffing boxes and extra long glands, so there can be no escaping of steam or gases and all oil bearings are located on the outside of the casing of the machine.

The outlets at the bottom, through which the condensed milk must pass, are fitted with test cocks so that samples of every run of milk may be taken, if desired, and thus an absolute check kept on the high quality of the product.

9

·				
Q				
			•	
	•	,		
,				



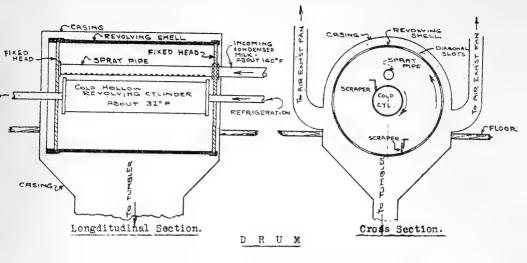
- . 1. Milk enters from the degermer through the pipes shown at the top.
  - 2. It is spread and evenly distributed by passing through the small holes in the spread pipes.
  - The milk now flows slowly in a very thin sheet, over the heated and slightly inclined corrugated plates, the temperature rising to approximately 90 degrees F.
  - 4. It now falls from the plates to the upper or first hot rollers (one on each side), and passes half way round the same in an even layer about 1/32" thick, at the same time rising to about 140 degrees and giving off part of its moisture which is immediately absorbed by the hot dry air passing through the apparatus at a high speed.
  - The milk is next forced from the under side of the hot rollers to the cold rollers. This is accomplished by the knife-edge scrapers.
  - 6. It passes half way around the cold rollers and is thus slightly cooled.
  - It is again scraped off and passes to the next hot rollers, where evaporation is again caused with the temperature reaching 140 F.
  - 8. The milk is again cooled on the cold roller.
  - 9. It now passes over the final (bottom) hot rollers where more moisture is evaporated at the temperature stated above. Scraper blades force it from these rollers as from the preceding ones to prevent boiling, burning or overheating.

About 75% of the moisture in the milk has now been evaporated without the milk at any time being overheated, the immense volumes of hot dry air passing over the rollers greatly assisting in the process of evaporation. The milk is now the consistency of condensed milk, and may, if desired, be sold as such, after passing through a re-vitalizing process with pure filtered air.

If milk powder is to be made, the re-vitalized condensed milk passes to the drum, described on the following sheet.

No milk is allowed to accumulate in the bottom of the evaporator, the product being forced, by air blast, into the re-vitalizing tank as fast as it falls from the bottom rollers.





The drum shown herewith consists of a revolving shell running on the two fixed heads, with a light metal casing enclosing the entire apparatus. This shell is driven by gear wheels, not shown.

The condensed milk from the re-vitalizing tank is forced into the spread pipe by compressed air heated to a high temperature, and is spread in fine streams, at a temperature of approximately 140 F, on to the hollow revolving cylinder, which is kept to about 32 degrees F by refrigeration. The heat contact is very limited.

The heated milk, coming in sudden contact with the very cold surface of the roller, instantly congeals the milk into ribbons and strips.

These ribbons and strips are continually scraped from the cold roller and the inner surface of the revolving shell (upon which they subsequently fall) and carried through slots in the revolving shell to be passed into the tumbler.

The latter, which is a very simple apparatus for breaking up the ribbons and strips, is located immediately under the drum. Hot dry air is forced through this tumbler in great quantities to further dry out the milk. It is drawn off by the air exhaust fan through the two pipes shown in the cross section.

Tumbler and drum have the same capacity as the evaporator, so that no storing of the condensed milk will be required.

# COST OF MACHINERY

Evaporator Drum Tumbler Degermer 2 Pulverizers at \$1,140.00. Air heater box and pipe coils Air exhaust fan Air compressor. Air receiver tank Revitalizing tank Flow regulating tank Steam and water piping Hot dry air piping	250.00 50.00 150.00 2,280.00 50.00 350.00 25.00 25.00 25.00 50.00 100.00
Hot dry air piping. Millwrighting (shafting, pulleys, etc.). Machinery foundations. Expection of machinery.	100.00 150.00 300.00 500.00
Additional working capital.  Grand Total	\$5.375.00 1,625.00 \$7,000.00

being given as maximum, the actual cost will be less than total of \$5,375.)

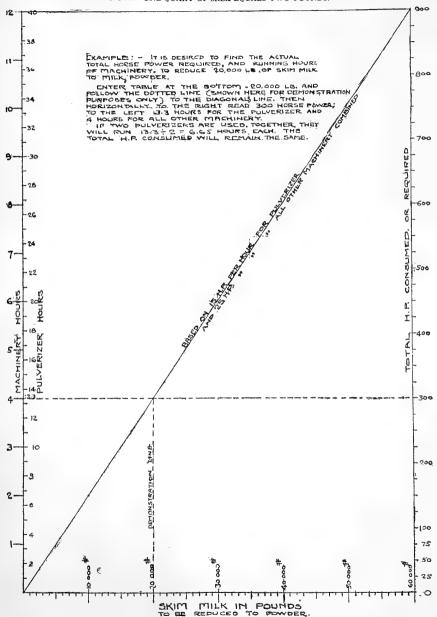
(Estimated costs

NOTE.—It is assumed that the plant is annexed to a creamery which will furnish the power required, steam heat, refrigeration, pure fresh water, etc.

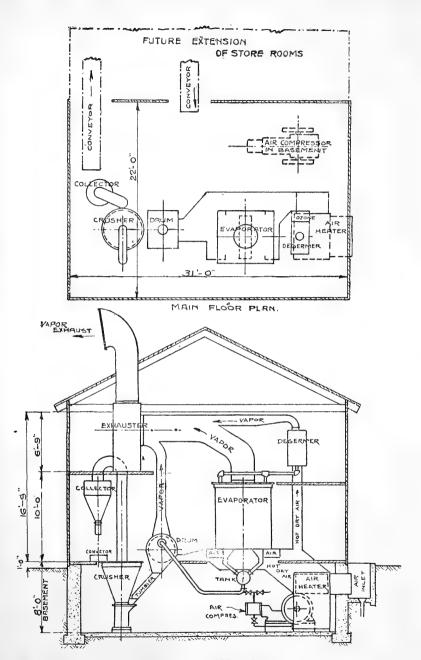


# DIAGRAM FOR CALCULATING RUNNING TIME OF MACHINERY AND TOTAL H. P. CONSUMED FOR ANY OUANTITY OF MILK FROM 1 TO 60,000 LBS. INCLUSIVE.

NOTE:-ONE QUART OF MILK EQUALS TWO POUNDS.



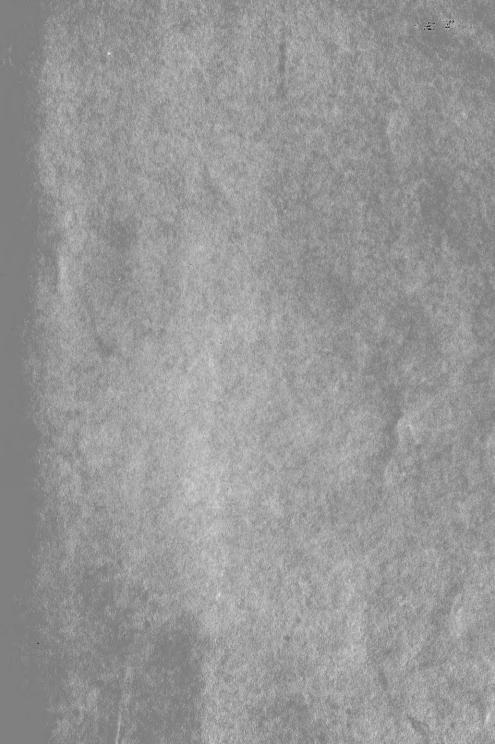




CROSS - SECTION



SOME MILK POWDER PRODUCTS					
	PRODUCT	USE	PACKED IN	SOLD TO	METHOD
1	MILK POWDER	General	Barrels	Bakers Confectioners	Direct
2	MILK FLOUR	Home Use	Cartons	Grocery Trade	Jobbers
3	MILK FLAKES		"		"
4	MILK DOMINO CRYSTALS	44	44	"	44
5	MILK JELLY	"	Glass Jars	"	"
6	MILK CUBES	Tourists Soldiers	Tins	Grocers Confectioners	44
7	MILK GRANULES	Infants Invalids	Bottles	Drug Trade	
8	MILK POWDER CAPSULES	Invalids	Glass Jars		66
9	MILK WAFERS	Confectioners	Wax Paper	Druggists Confectioners	44
10	MILK STICKS	44	4.6		"
11	MILK FLESH FOOD	General	Boxes	Drug Trade	
12	TOILET MILK PREPARATIONS	44	6.6	**	**



LIBRARY OF CONGRESS 0 000 891 022 4